

AMENDMENTS TO THE CLAIMS

We claim:

1. (currently amended) A process for preparing maleic anhydride by comprising: oxidizing n-butane in the gas phase under heterogeneous catalysis with oxygen-containing gases over a vanadium-, phosphorus- and oxygen-containing catalyst in a reactor unit at a temperature in the range from 350 to 500°C[,] ; and removing the maleic anhydride formed to form a gas stream which comprises unconverted n-butane and water and recycling at least a portion of the unconverted n-butane to the reactor unit, which comprises ; wherein the process further comprises: feeding to the reactor unit an inlet stream having an n-butane concentration of from 0.5 to 1.5% by volume and an oxygen concentration of from 5 to 21% by volume[,] ; establishing a pressure at the inlet to the reactor unit of from 0.4 to 2 MPa abs[,] ; and converting from 40 to 100% of the n-butane from the inlet stream per reactor pass.
2. (original) A process as claimed in claim 1, wherein an inlet stream having an n-butane concentration of from 1 to 1.5% by volume is fed to the reactor unit.
3. (currently amended) A process as claimed in either of claims 1 and 2 claim 1, wherein an inlet stream having an oxygen concentration of from 10 to 18% by volume is fed to the reactor unit.
4. (currently amended) A process as claimed in any of claims 1 to 3 claim 1, wherein an inlet stream having a pressure of from 0.4 to 1 MPa abs is fed to the reactor unit.
5. (currently amended) A process as claimed in any of claims 1 to 4 claim 1, wherein a GHSV of from 2000 to 10 000 h⁻¹, based on the volume of the inlet stream fed, normalized to 0°C and 0.1013 MPa abs, and based on the bed volume of the catalyst summed over all reaction zones, is established in the reactor unit via the flow rate of the inlet stream.
6. (currently amended) A process as claimed in any of claims 1 to 5 claim 1, wherein the oxygen-containing gas used is air.

phase oxidation is carried out in the presence of a volatile phosphorus compound.

8. A process as claimed in any of claims 1 to 7, wherein the reactor unit used is a fluidized bed reactor unit.
9. A process as claimed in any of claims 1 to 7, wherein the reactor unit used is a tube bundle reactor unit having at least one reaction zone cooled by a heat carrier medium.
10. A process as claimed in claim 9, wherein a tube bundle reactor unit is used which has at least two reaction zones cooled by a heat carrier medium.
11. A process as claimed in any of claims 1 to 10, wherein at least 40% of the unconverted n-butane is recycled to the reactor unit.
12. A process as claimed in claim 11, wherein from 40 to 80% of the unconverted n-butane is recycled to the reactor unit.
13. A process as claimed in any of claims 1 to 12, wherein maleic anhydride is removed from the gas stream withdrawn from the reactor unit and at least a portion of the gas stream depleted in maleic anhydride is recycled to the reactor unit.
14. (new) A process as claimed in either of claim 2, wherein an inlet stream having an oxygen concentration of from 10 to 18% by volume is fed to the reactor unit.
15. (new) A process as claimed in any of claim 2, wherein an inlet stream having a pressure of from 0.4 to 1 MPa abs is fed to the reactor unit.
16. (new) A process as claimed in any of claim 3, wherein an inlet stream having a pressure of from 0.4 to 1 MPa abs is fed to the reactor unit.
17. (new) A process as claimed in any of claim 4, wherein a GHSV of from 2000 to 10 000 h⁻¹, based on the volume of the inlet stream fed, normalized to 0°C and 0.1013 MPa abs, and based on the bed volume of the catalyst summed over all reaction zones, is established in the reactor unit via the flow rate of the inlet stream.

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18. (new) A process as claimed in any of claim 3, wherein a GHSV of from 2000 to 10 000 h⁻¹, based on the volume of the inlet stream fed, normalized to 0°C and 0.1013 MPa abs, and based on the bed volume of the catalyst summed over all reaction zones, is established in the reactor unit via the flow rate of the inlet stream.
19. (new) A process as claimed in claim 4, wherein a GHSV of from 2000 to 10 000 h⁻¹, based on the volume of the inlet stream fed, normalized to 0°C and 0.1013 MPa abs, and based on the bed volume of the catalyst summed over all reaction zones, is established in the reactor unit via the flow rate of the inlet stream.
20. (new) A process as claimed in claim 2, wherein the oxygen-containing gas used is air.